

# Sunlight Powered Continuous Flow Reverse Water Gas Shift Process Using a Plasmonic Au/TiO<sub>2</sub> Nanocatalyst

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**Abstract:** The continuous flow reverse water gas shift (rWGS) process was efficiently catalyzed by a plasmonic Au/TiO<sub>2</sub> nanocatalyst using sunlight as sole and sustainable energy source. The influence of the catalyst bed thickness on the CO production rate was studied, and three different catalytic regimes were identified as direct plasmon catalysis (DPC), shielded plasmon catalysis (SPC) and unused plasmon catalysis (UPC). The CO<sub>2</sub>:H<sub>2</sub> ratio was optimized to 4:1 and a maximum CO production rate of 7420 mmol·m<sup>-2</sup>·h<sup>-1</sup> was

achieved under mild reaction conditions ( $p=3.5$  bar, no external heating,  $E_e=14.0$  kW·m<sup>-2</sup>), corresponding to an apparent quantum efficiency of 4.15%. The stability of the Au/TiO<sub>2</sub> catalyst was studied for 110 h continuous operation, maintaining more than 82% of the initial CO production rate. On/off experiments mimicking discontinuous sunlight powered processing furthermore showed that the Au/TiO<sub>2</sub> catalyst was stable for 8 consecutive runs.

## Introduction

CO<sub>2</sub> capture and utilization (CCU) technologies are expected to play an important role in the near future to produce platform chemicals, polymers, and synthetic fuels to power e.g. heavy transport and aviation.<sup>[1]</sup> Technically scalable and economically feasible CCU concepts are required to achieve a fully defossilized carbon economy. In the past decades, several CO<sub>2</sub> conversion technologies have been explored, such as biocatalytic, electrochemical, photo(electro)chemical and thermochemical processes.<sup>[1–2]</sup> Photochemical processes are attractive because of their potential for direct use of sunlight as sustainable energy source and their typical clean production under mild reaction conditions.<sup>[3]</sup> To achieve efficient sunlight utilization and high production rates, plasmonic metal nanoparticles (NPs) have been applied as catalysts, in specific cases in combination with a semiconductor.<sup>[4]</sup> Plasmonic NPs can efficiently harvest sunlight because of their localized surface plasmon resonance (LSPR).<sup>[5]</sup> The light frequency at which a metallic NP experiences its LSPR depends amongst others on the nature of the metal,

size and shape of the NP and the distance between NPs.<sup>[6]</sup> Furthermore, supported metallic NPs can serve as catalysts, offering a large number of active sites on their chemically reactive surface.

CO<sub>2</sub> can be reduced to chemicals and fuels via catalytic hydrogenation, leading to products such as CH<sub>4</sub> and CO.<sup>[7]</sup> CH<sub>4</sub> is produced in the Sabatier reaction (Eq. 1), whilst CO is obtained by the reverse water gas shift (rWGS) process (Eq. 2). Syngas, a mixture of CO and H<sub>2</sub>, can be applied to produce methanol, and long chain hydrocarbons using Fischer-Tropsch synthesis.<sup>[8]</sup> Therefore, the rWGS reaction can serve as first step for the production of synthetic fuels and chemicals from CO<sub>2</sub>.



The rWGS reaction is endothermic and limited by equilibrium.<sup>[9]</sup> In thermocatalysis temperatures above 800 °C are required to produce CO with a selectivity above 80%.<sup>[10]</sup> At lower temperatures, CH<sub>4</sub> production is favoured. As alternative to the thermocatalytic process, plasmonic catalysis aims to use metallic NPs, to harvest the energy of (sun)light and use it to drive the reaction. When metallic nanoparticles are exposed to light, free electrons display a resonant response based on the localized surface plasmon resonance (LSPR). This coherent oscillation dephases and generates hot electrons, which can promote the rWGS reaction in three main ways: (1) they can be transferred to unoccupied molecular orbitals of reactants adsorbed on the surface of the metal nanocatalyst to induce bond dissociation (non-thermal contribution), (2) they can be injected into the conduction band of the semiconductive support and thereby enhance the photocatalytic activity of the semiconductor (non-thermal contribution), and (3) they can thermalize via electron-electron and electron-phonon scatter-

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ing, resulting in an increased temperature of the catalyst (photothermal contribution).

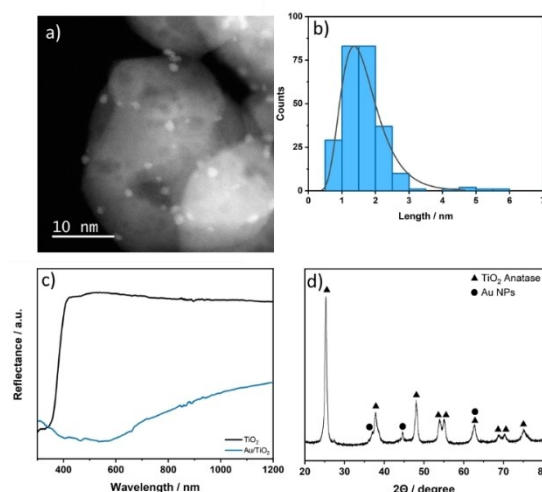
Supported noble metal nanocatalysts based on Au have been reported to reach the highest activities in the light powered rWGS reaction. Huber *et al.* studied the performance of Au NPs supported on different metal oxides at 400 °C and visible light irradiation ( $5216 \text{ W} \cdot \text{m}^{-2}$ ), reporting a  $\text{CO}_2$  conversion rate of  $2663 \mu\text{mol} \cdot \text{g}_{\text{cat}}^{-1} \cdot \text{min}^{-1}$ .<sup>[11]</sup> Several catalysts based on Au and Ag NPs supported on  $\text{TiO}_2$  were studied by Tahir *et al.*, unravelling the potential of different  $\text{TiO}_2$  morphologies and the use of bimetallic catalysts. They investigated Au/ $\text{TiO}_2$  nanostructures, with maximum activity of  $4144 \mu\text{mol} \cdot \text{g}_{\text{cat}}^{-1} \cdot \text{h}^{-1}$  under  $150 \text{ mW} \cdot \text{cm}^{-2}$  irradiance.<sup>[12]</sup> Bobadilla *et al.* recently studied the role of oxygen vacancies in the rWGS reaction, and proposed a redox mechanism for Au/ $\text{TiO}_2$  catalysts with involvement of  $\text{Ti}^{3+}$  species.<sup>[13]</sup> They suggested the formation of hydroxy carbonyl intermediates, which further decompose to CO and water. Alternative metals, such as Ag, Fe and Cu also catalyse the light-powered rWGS reaction, albeit with lower activity.<sup>[14]</sup> Other metals, such as Ru and Ni have shown a strong selectivity towards  $\text{CH}_4$  production.<sup>[7a,d,h,15]</sup> Recently, our group has reported plasmonic Au nanoparticles supported on  $\text{TiO}_2$  that promote the rWGS reaction under sunlight irradiation without any external heating in a batch process.<sup>[7e,f]</sup> We reported a maximum CO initial production rate of  $429 \text{ mmol} \cdot \text{g}_{\text{Au}}^{-1} \cdot \text{h}^{-1}$  ( $8525 \text{ mmol} \cdot \text{m}^{-2} \cdot \text{h}^{-1}$ ) with a selectivity of 98% and an apparent quantum efficiency of 4.7% using mildly concentrated sunlight ( $1.44 \text{ W} \cdot \text{cm}^{-2} = 14.4$  suns) in a batch process.

To scale up and progress towards an industrially applicable technology, is of vital importance (i) to transfer from a batch to a continuous flow process and (ii) to maximize the CO production rate per  $\text{m}^{-2}$  illuminated catalyst bed to minimize land use. Furthermore, it is crucial to study (iii) the catalyst stability over a prolonged period of time and (iv) in on-off experiments to mimic discontinuous sunlight powered production. In this study, we address these four challenges for the sunlight powered rWGS process.

## Results and discussion

### Catalyst synthesis and characterization

The Au/ $\text{TiO}_2$  catalyst was synthesized via a deposition-precipitation method reported previously and described in more detail in the experimental section and previously reported.<sup>[7e]</sup> The Au loading was analyzed through Inductively Coupled Plasma-Atomic Emission Spectroscopy (ICP-AES), yielding a Au content of 3.1 wt.%. Representative High-Angle Annular Dark Field-Scanning Transmission Electron Microscopy (HAADF-STEM) images display  $\text{TiO}_2$  nanoparticles decorated with small Au nanospheres (Figure 1a). The average Au particle size was determined by measuring 200 NPs, resulting in an average diameter of 1.70 nm, and following a lognormal distribution (Figure 1b). The diffuse UV-visible reflectance spectra showed a large difference between the  $\text{TiO}_2$  anatase support and the Au/ $\text{TiO}_2$  catalyst (Figure 1c). In the first case, light absorption was

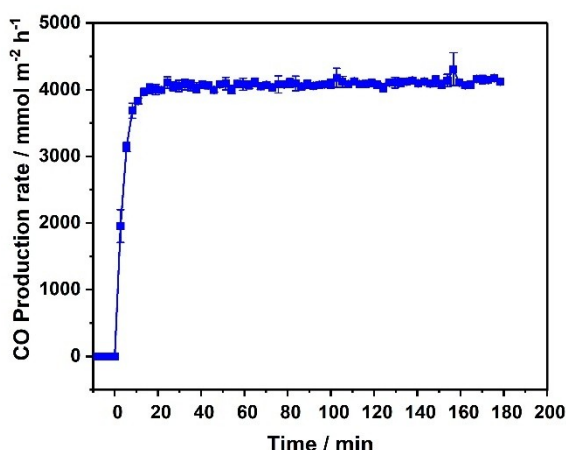


**Figure 1.** Characterization of the Au/ $\text{TiO}_2$  catalyst. a) Representative HAADF-STEM image of the Au/ $\text{TiO}_2$  catalyst showing the Au NPs on the  $\text{TiO}_2$  support; b) Particle size distribution histogram; c) Diffuse reflectance UV-Vis-NIR spectra for  $\text{TiO}_2$  (black curve) and Au/ $\text{TiO}_2$  (blue curve); d) XRD pattern of the Au/ $\text{TiO}_2$  nanocatalyst [ $\text{TiO}_2$  01-073-1764, Au 00-004-0784].

only achieved above the bandgap of  $\text{TiO}_2$  in the UV region, while in the second case the absorption was broadened to the visible spectrum based on the LSPR of the Au nanoparticles. The powder X-ray diffraction (XRD) analysis confirmed the crystallinity of the anatase  $\text{TiO}_2$  support, and displayed peaks at  $38.2^\circ$ ,  $44.4^\circ$  and  $64.5^\circ$  of metallic Au (Figure 1d).

### Sunlight powered continuous flow rWGS process

The  $\text{CO}_2$  photoreduction experiments were performed in a tailored photoreactor system. The reactor was irradiated through a quartz window on top.  $\text{N}_2$  was used as internal standard. The applied light source was a solar simulator (Newport Sol3A) equipped with an AM1.5 filter, with a tuneable light intensity up to  $14 \text{ kW} \cdot \text{m}^{-2}$  ( $= 14$  suns). To measure the catalyst bed temperature, a thermocouple placed in contact with the bottom of the catalyst bed ( $T_c$ ) was used. A scheme of the system is provided in the ESI Figure S2. The reactor temperature was measured using a second thermocouple ( $T_r$ ). In the experiments under illumination, simulated sunlight was used as sole energy source without additional external heating of the reactor. Time zero was defined as the moment when the light was switched on. In line with our previous work on the rWGS batch process, we performed the continuous flow process at a pressure of 3.5 bar to ensure an overpressure in the reactor and prevent air from entering. In the thermocatalytic reference experiments (dark experiments), no light irradiation was used and the reactor was heated via electric heating rods. The reactant mixture was introduced after thermal equilibrium when the desired temperature was achieved, and this instance was considered time zero. This was done to avoid catalyst deactivation during the process of reactor heating. Since the rWGS reaction is limited by equilibrium and the temperature of

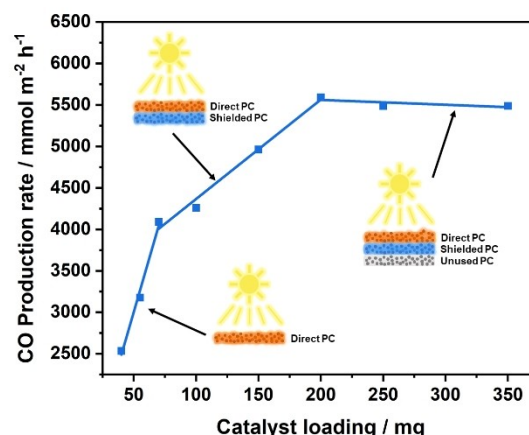


**Figure 2.** Average CO production rate with standard deviation as function of time. 75 mg Au/TiO<sub>2</sub> catalyst was loaded on the 3.14 cm<sup>2</sup> area designed for the catalyst bed holder using a 1:1 CO<sub>2</sub>:H<sub>2</sub> ratio. Reaction conditions: 3.5 bar, total flow 135 mL·min<sup>-1</sup>, 14.0 suns irradiation from solar simulator (1 sun = 1 kW·m<sup>-2</sup>, AM1.5) without external heat.

the catalyst bed is rather low in our study (always below 200 °C), the CO<sub>2</sub> conversion is always below 5%. This ensures that we are not operating in a regime in which mass transfer is limiting the conversion rate. A continuous flow experiment under 14 suns irradiation without external heating was performed. This experiment was carried out *in triplo* to determine the experimental error. Using a CO<sub>2</sub>:H<sub>2</sub> ratio of 1:1, the obtained CO production rate was  $4086 \pm 57$  mmol·m<sup>-2</sup>·h<sup>-1</sup> and the apparent quantum efficiency (AQE) was 3.2% (ESI S3). The selectivity for CO was 96.9% (Figure 2) and only CH<sub>4</sub> was detected as a side product. During the 3 hours duration of the continuous flow experiment, both the activity and the selectivity of the reaction remained constant, and no catalyst deactivation was observed.

### CO production rate: optimizing catalyst bed thickness

One of the main difficulties when comparing the performance of different plasmonic catalysts and results obtained by different labs is that there is not a standard protocol to test and report plasmon catalytic activities. Frequently, the catalytic activity is reported in mmol·g<sub>cat</sub><sup>-1</sup>·h<sup>-1</sup>. However, normalizing the production rate to the mass of the catalyst (or the mass of plasmonic metal) is not a useful normalization to compare different catalysts or results from different labs, because the reaction rate does not follow a linear increase with the photocatalyst mass due to the limited light penetration depth and corresponding shielding effect.<sup>[16]</sup> It is therefore better to report the catalytic activity per m<sup>2</sup> illuminated area. To optimize the thickness of the catalyst bed, we studied the relationship between the CO production rate and the catalyst mass placed on the 3.14 cm<sup>2</sup> holder. Using 40 mg of catalyst, the illuminated surface area was completely covered. The CO production rate for the various loadings shows three different regimes with a distinct transition from regime 1 to regime 2 at 70 mg, and

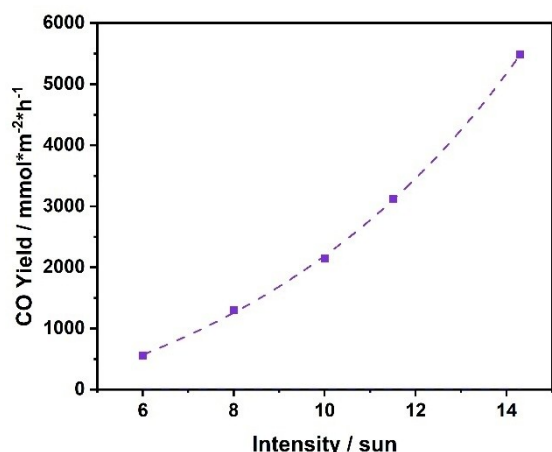


**Figure 3.** CO Production rate as function of catalyst loading on the 3.14 cm<sup>2</sup> holder designed for the Au/TiO<sub>2</sub> catalyst bed, and using a 1:1 CO<sub>2</sub>:H<sub>2</sub> ratio. Reaction conditions: 3.5 bar, total flow 135 mL·min<sup>-1</sup>, 14.0 suns irradiation from solar simulator. (1 sun = 1 kW·m<sup>-2</sup>, AM1.5) without external heat.

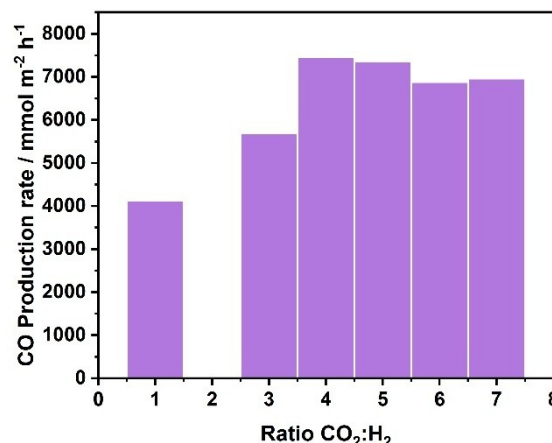
from regime 2 to regime 3 at 200 mg loading (Figure 3). Up to 70 mg, all the catalyst material is directly exposed to light. We designated this regime as direct plasmon catalysis (DPC). At higher loadings – between 70 mg and 200 mg – the slope change indicates that part of the catalyst is not directly exposed to light because of shielding, but can nevertheless contribute to the catalytic process, *e.g.* via absorption of (scattered) light of a lower irradiance, or via transfer of heat from the photothermally heated top surface to the layer below (shielded PC). Above 200 mg, the CO production rate reaches a plateau, meaning that further addition of catalyst does not increase the CO production rate because it is neither illuminated nor heated (unused PC). Should be noticed, that as reported previously by our group, there is a temperature gradient present inside the illuminated catalyst bed, because of single-side illumination and poor thermal conductivity.<sup>[17a]</sup>

### Photothermal vs. non-thermal contribution

To differentiate between photothermal and non-thermal contributors, the relationship between irradiance and the CO production rate was studied. When varying the irradiance, the rate of reactions solely initiated via a transfer of hot electrons to antibonding orbitals of adsorbed reactants displays a linear dependence on the irradiance, since the rate of the reaction is proportional to the photon flux. In contrast, photothermal reactions display an exponential relationship between the reaction rate and the irradiance, since the temperature of the catalyst is proportional to the light absorption and rate constants of chemical reactions typically follow an Arrhenius-type of temperature dependence. As shown in Figure 4, the CO production rate increases exponentially when the light intensity is raised from 6 to 14 suns. However, the catalyst bed temperature increases linearly from 78 °C to 152 °C as can be



**Figure 4.** CO Production rate as function of irradiance. Reaction conditions: 200 mg Au/TiO<sub>2</sub>, 1:1 CO<sub>2</sub>:H<sub>2</sub> ratio, 3.5 bar, total flow 135 mL·min<sup>-1</sup> without external heat.



**Figure 5.** Effect of the CO<sub>2</sub>:H<sub>2</sub> ratio. Reaction conditions: 70 mg Au/TiO<sub>2</sub>, 3.5 bar, total flow 135 mL·min<sup>-1</sup>, 14.0 sun irradiation from solar simulator. (1 sun = 1 kW·m<sup>-2</sup>, AM1.5), without external heat.

observed in Figure S14 in the ESI. There is a temperature gradient present inside the illuminated catalyst bed, because of single-side illumination and poor thermal conductivity.<sup>[17]</sup> For a more accurate determination of  $E_{A_r}$ , the temperature at various depths inside the catalyst bed should be monitored *in operando*, for which no technology is available to date. The observed exponential relationship demonstrates that the main contributor to this process is photothermal heating, but does not exclude an additional photochemical contributor. In a previous study, we have concluded that Au NPs are mainly responsible for the light absorption and the promotion of the reaction, since UV light above the bandgap of TiO<sub>2</sub> had no significant influence on the process.<sup>[7d]</sup>

### Effect of the CO<sub>2</sub>:H<sub>2</sub> ratio

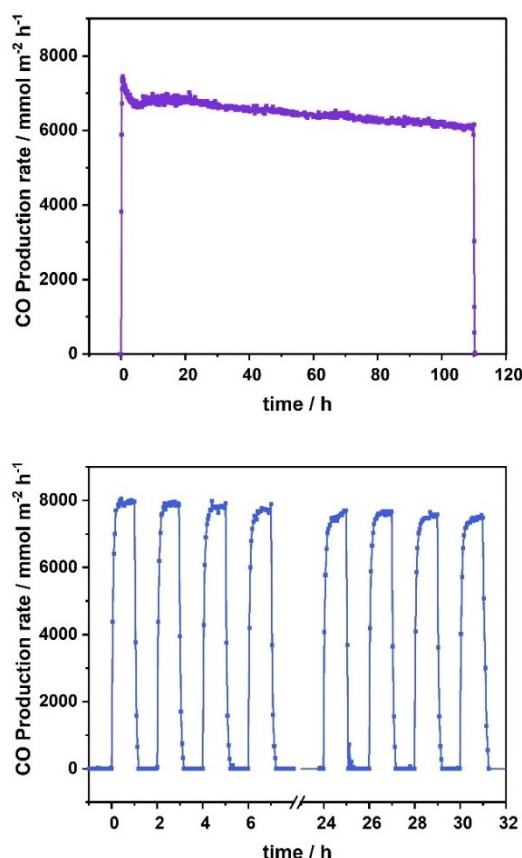
The dependence of the CO production rate on the CO<sub>2</sub>:H<sub>2</sub> ratio was studied for 6 different feedstock compositions (ESI S5) from the stoichiometric ratio (1:1) to CO<sub>2</sub> excess of (7:1). The total flow rate was kept constant as we varied the CO<sub>2</sub> share in the starting gas mixture from 44.4% for the ratio (1:1) to 77.8% for the ratio (7:1), whilst keeping the N<sub>2</sub> share constant at 11.1% (ESI table S5). The CO production rate shows an increase when increasing the CO<sub>2</sub>:H<sub>2</sub> ratio (Figure 5) until reaching a maximum at CO<sub>2</sub>:H<sub>2</sub> ratio of 4:1–5:1, achieving a CO production rate of 7423 mmol·m<sup>-2</sup>·h<sup>-1</sup> which corresponds to an AQE of 4.15%. At higher ratios, the CO production rate slightly decreases. The CO selectivity remained constant between the different reactant ratios, and was always higher than 96%. An important contributor to the increase in reaction rate with increasing CO<sub>2</sub>:H<sub>2</sub> ratio is the increase in catalyst bed temperature. The catalyst bed temperature increases linearly with increasing CO<sub>2</sub>:H<sub>2</sub> ratio from 134 °C (ratio of 1:1) to 141.5 °C (ratio of 7:1) (ESI Figure S15). This can be attributed to the lower thermal conductivity of CO<sub>2</sub> when compared to H<sub>2</sub>. The catalyst surface temperature should be much higher, and this temperature

should be monitored *in operando*, for which no technology is available to date.

Thermocatalytic experiments (dark experiments) were performed as reference experiments to compare the catalytic activity and selectivity to the experiments under light. The reactor was heated from the laterals using electrical heating rods. The system reached the desired temperature under N<sub>2</sub> flow and was then filled with the reactants in order to avoid catalyst deactivation during the heating process. The CO production rate was studied from 140 °C to 200 °C using a 4:1 CO<sub>2</sub>:H<sub>2</sub> ratio, 70 mg of Au/TiO<sub>2</sub> catalyst, 3.5 bar pressure and a total flow of 135 mL·min<sup>-1</sup> (See Figure S6 in the ESI). The CO production rate increases exponentially with rising temperature. The CO production rate achieved in dark at 200 °C was 3716 mmol·m<sup>-2</sup>·h<sup>-1</sup> at CO selectivity of 80%, with CH<sub>4</sub> as sole side product. The activity and selectivity are significantly lower when compared to the illuminated counterpart, viz. 3716 mmol·m<sup>-2</sup>·h<sup>-1</sup> (dark, 200 °C) vs. 7423 mmol·m<sup>-2</sup>·h<sup>-1</sup> (light, 14 suns) and 80% (dark, 200 °C) vs. 96% (light, 14 suns), respectively. We propose that the difference in selectivity could be caused by the promotion of H<sub>2</sub>O and CO desorption through charge transfer of plasmon generated charges, limiting further reduction to CH<sub>4</sub>.

### Catalyst stability

The catalyst stability in the continuous flow sunlight powered rWGS process was studied for 110 h. The first 24 h showed a production decrease until reaching 90% of the initial CO production (Figure 6a). After 110 h we still observed more than 82% of the initial CO production without displaying any abrupt deactivation. The minor gradual deactivation may be attributed to H<sub>2</sub>O accumulation in the photoreactor, since the reactor itself remains at room temperature. The spent catalyst was characterized to investigate whether morphology changes occurred during the reaction. As determined by HAADF-STEM analyses,



**Figure 6.** Catalyst stability test. a) CO production rate as function of time, b) on-off test where the solar simulator was turned on/off every hour. Reaction conditions: 70 mg Au/TiO<sub>2</sub>, 4:1 CO<sub>2</sub>:H<sub>2</sub> ratio, 3.5 bar, total flow 135 mL·min<sup>-1</sup>, 14.0 sun irradiation from solar simulator. (1 sun = 1 kW·m<sup>-2</sup>, AM1.5) without external heat.

the average Au particle size was 1.82 nm following a lognormal distribution (ESI S7, Figure S7a–b). This Au nanoparticle size does not significantly deviate from the initial value of 1.70 nm. This indicates a good structure stability during the 110 h experiment with no signs of catalyst sintering.

The high selectivity of the catalyst could be attributed to promotion of CO desorption through charge transfer of plasmon generated charges, as suggested in previous studies.<sup>[7e,11,18]</sup> In dark reference experiments, the selectivity is substantially lower due to further hydrogenation of adsorbed CO to CH<sub>4</sub>. The difference in activity between the light-powered and thermal rWGS reaction may be caused by the difference in surface temperature of the illuminated catalyst bed and the temperature measured by the thermocouple in contact with the bottom of the catalyst bed. As shown in a previous study, this difference may be of the order of 150 °C.<sup>[17a]</sup> The high stability of the catalyst is related to the rather low operating temperature.

Since solar irradiation fluctuates over time, the CO production rate and the catalyst stability was further investigated by performing on/off experiments. Stopping and starting the process can have a substantial impact on the catalytic performance. Light was switched on during 1 h, switched off for one

hour, for 4 consecutive cycles. Afterwards, the reactor was off overnight and the next day 4 extra cycles were performed. After 4 cycles, the CO production rate was similar to the first cycle (98%, 7888 mmol·m<sup>-2</sup>·h<sup>-1</sup>). After the 4<sup>th</sup> cycle the catalyst remained at RT in dark overnight (17 h). The next day in the 5<sup>th</sup> cycle we achieved 96% of the starting production rate (7694 mmol·m<sup>-2</sup>·h<sup>-1</sup>) after 1 h under illumination. The initial CO production rate was lower, most probably due to the remained adsorbed water on the catalyst bed. The 8<sup>th</sup> cycle had a production rate of 7567 mmol·m<sup>-2</sup>·h<sup>-1</sup> that corresponded to 94% of the CO production rate obtained in the first cycle.

## Conclusions

In conclusion, the present study shows that plasmonic Au/TiO<sub>2</sub> nanocatalysts are efficient in the rWGS process using sunlight as sole and sustainable energy source. To scale up and progress towards an industrially applicable technology, we successfully transferred from a batch to a continuous flow process. Furthermore, we studied the effect of the catalyst layer thickness on the CO production rate, and three regimes were identified as DPC, SPC and UPC. The results are applied to maximize the CO production rate per m<sup>2</sup> illuminated catalyst bed to minimize land use. Under optimized conditions, we achieved a CO production rate of 7423 mmol·m<sup>-2</sup>·h<sup>-1</sup> and a selectivity of 96%, which corresponded to an AQE of 4.15%. Both activity and selectivity were significantly higher for the sunlight-powered process when compared to thermal reference experiments in dark, viz. 3716 mmol·m<sup>-2</sup>·h<sup>-1</sup> (dark, 200 °C) vs. 74230 mmol·m<sup>-2</sup>·h<sup>-1</sup> (light, 14 suns) and 80% (dark, 200 °C) vs. 96% (light, 14 suns), respectively. Furthermore, we demonstrated that the catalyst was stable, both over a prolonged period of time (82% activity remained after 110 h) and in on-off experiments to mimic discontinuous sunlight powered production (94% activity remained after 8 cycles).

## Experimental

**Synthesis of the Au/TiO<sub>2</sub> catalyst.** The Au/TiO<sub>2</sub> catalyst was synthesized by a deposition-precipitation method, based on previously reported methodologies.<sup>[19]</sup> HAuCl<sub>4</sub>·3H<sub>2</sub>O (Sigma Aldrich, 99.9%) was used as the Au precursor. The Au precursor (200 mg) was added to ultra-filtered water (Milli-Q Millipore, 18.2 MΩ cm, 100 mL) in vigorous stirring. Then, the pH of the solution was adjusted to 9 by adding NaOH (0.1 M). Once the pH stabilized, TiO<sub>2</sub> (1.00 g, 99.5% anatase, loLiTec Nanomaterials) was added to the mixture, followed by an adjustment of the pH back to 9. The dispersion was left in vigorous stirring for 48 hours at room temperature, keeping a continuous control of the pH with a pH meter. The solid was recuperated by filtration and extensively washed with ultra-filtered water (Milli-Q Millipore, 18.2 MΩ cm). Subsequently, the solid was dried in a vacuum oven at 100 °C for 2 hours and calcinated in a tube furnace at 200 °C in a 20:80 O<sub>2</sub>:Ar atmosphere for 4 h, following a heating ramp of 2 °C·min<sup>-1</sup>. For this whole study, 10 syntheses of 1 g were done and their products were mixed to reduce the influence of batch-to-batch variations on the photocatalytic tests. The characterization shown corresponds to the obtained mixture.

**Photocatalytic tests:** The sunlight-powered CO<sub>2</sub> hydrogenation tests were performed in a custom-made flow photoreactor, equipped with a quartz window at the top to allow the light irradiation. The solar simulator (Newport Sol3A) was placed above it and was equipped with a high flux beam concentrator (Newport 81030), and AM1.5 filter and the possibility to introduce cut-off filters. The irradiated area was about 3.14 cm<sup>2</sup> and was covered by the sample. The reactor has three thermocouples to measure the temperatures at the top and bottom of the reactor, and under the catalyst bed. A schematic representation of the reactor setup can be seen in ESI Figure S2. In a typical run, 70 mg of the catalyst was put in the reactor, after removing the air with three times with N<sub>2</sub> and vacuum purge cycles, the reactor was filled with a mixture of H<sub>2</sub> (Linde 6.0), CO<sub>2</sub> (Linde 4.5) and N<sub>2</sub> (Linde 5.0), with a H<sub>2</sub>:CO<sub>2</sub>:N<sub>2</sub> flow of 24:96:15 mLmin<sup>-1</sup>, with the pressure regulated at 1.85 using a back pressure controller. The time 0 is considered when light was switched on. For dark experiments, the reactor was heated up until the desired temperature under nitrogen flow, and when the temperature was stable the CO<sub>2</sub> and H<sub>2</sub> were introduced. The products were analyzed by a gas chromatograph (Compact GC, Global Analyzer Solutions), which was directly coupled to the output of the reactor. The GC was equipped with three channels, two microthermal conductivity detectors (TCD) and one flame ionization detector (FID). The peak areas were used to determine the ratio of each compound based on calibration, using N<sub>2</sub> as an internal standard. If products were present in the time zero analysis, this value was subtracted from the measurements in the following times.

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## Conflict of Interests

There are no conflicts to declare.

## Data Availability Statement

The data that support the findings of this study are available from the corresponding author upon reasonable request.

**Keywords:** Carbon dioxide • photochemistry • reverse Water gas Shift flow • solar light • surface plasmon resonance

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