

Indirect vs. Direct Gasification

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INDIRECT *vs.* DIRECT GASIFICATION

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GASIFICATION

matching energy consumption and production

energy production:

fuel + air ($\lambda > 1$) \rightarrow flue gas + heat

25%

energy consumption:

fuel + heat \rightarrow gas + char/coke

75%

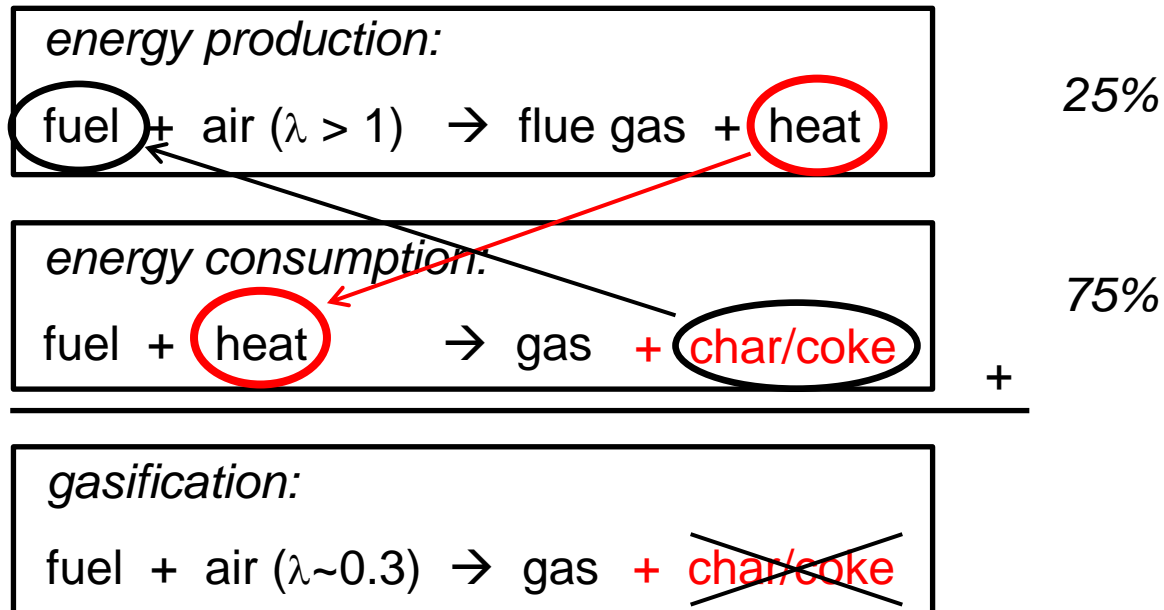
+

gasification:

fuel + air ($\lambda \sim 0.3$) \rightarrow gas + char/coke

SECOND GENERATION

also called: indirect gasification

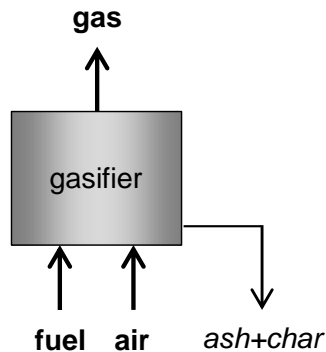


GASIFICATION

generations

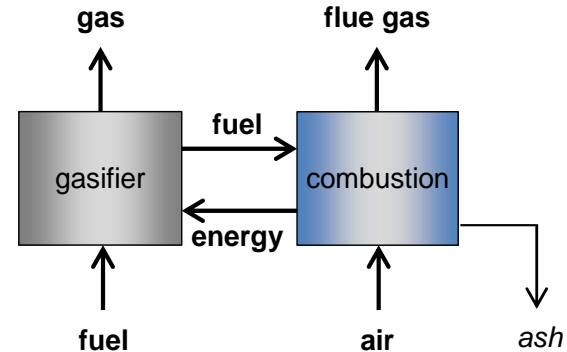
First generation (=direct)

- One reactor, one gas
- N₂-free gas requires ASU
- Incomplete carbon conversion
- High temperature, high steam, small fuel size, large residence time needed for acceptable conversion



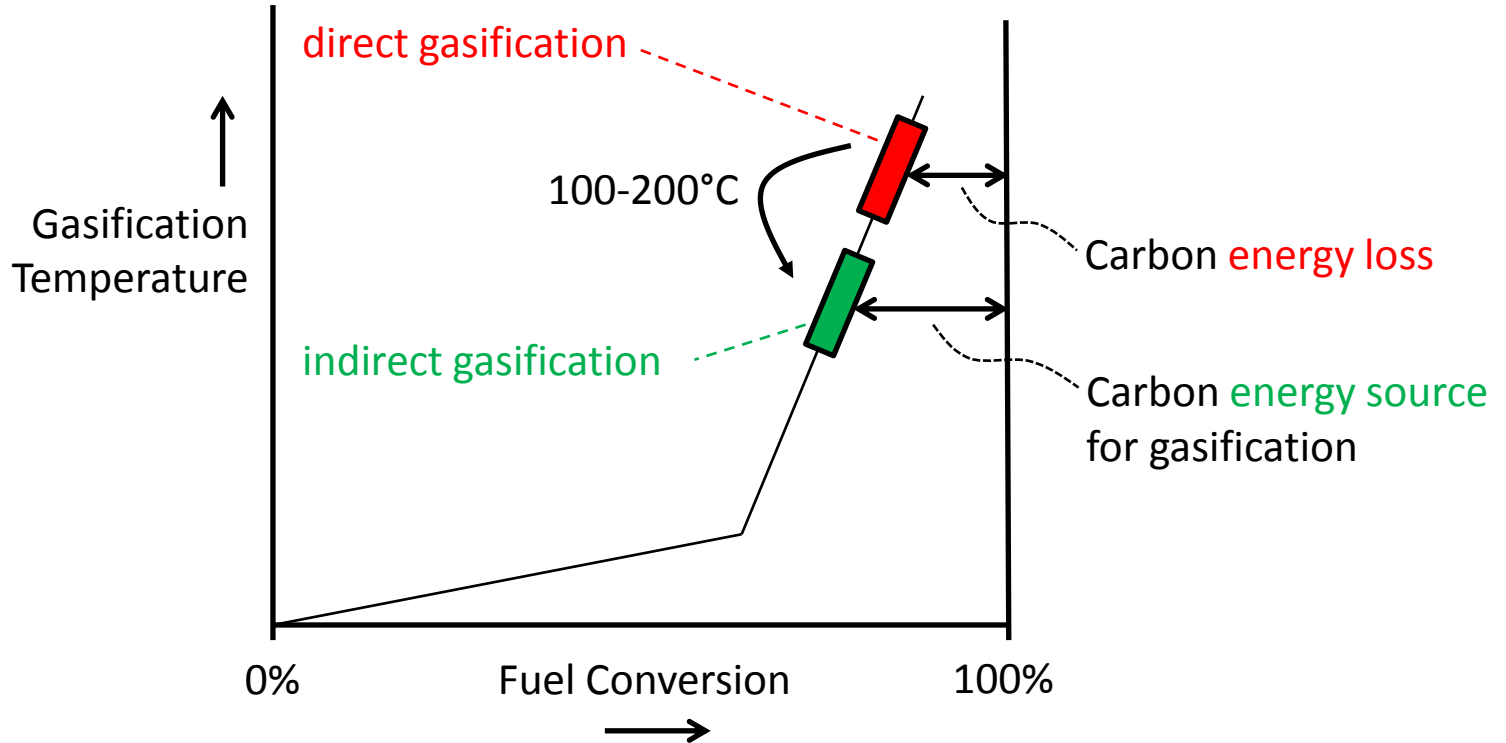
Second generation (=indirect)

- Two coupled reactors, two gases
- N₂-free gas without ASU
- Complete carbon conversion
- Additional degree of freedom: temperature, steam, fuel size, residence time



IN OTHER WORDS

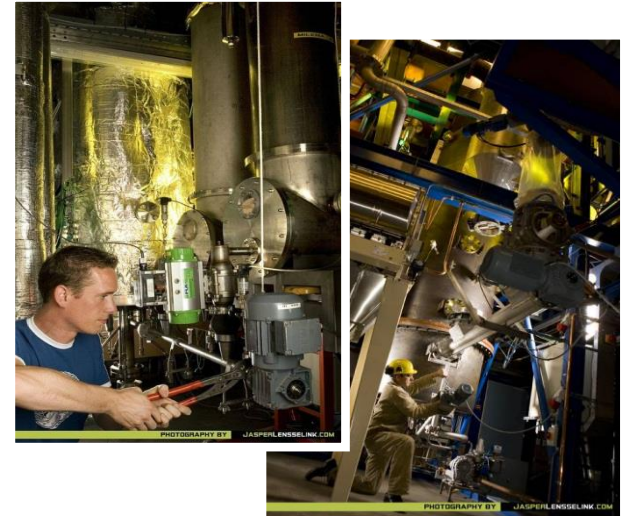
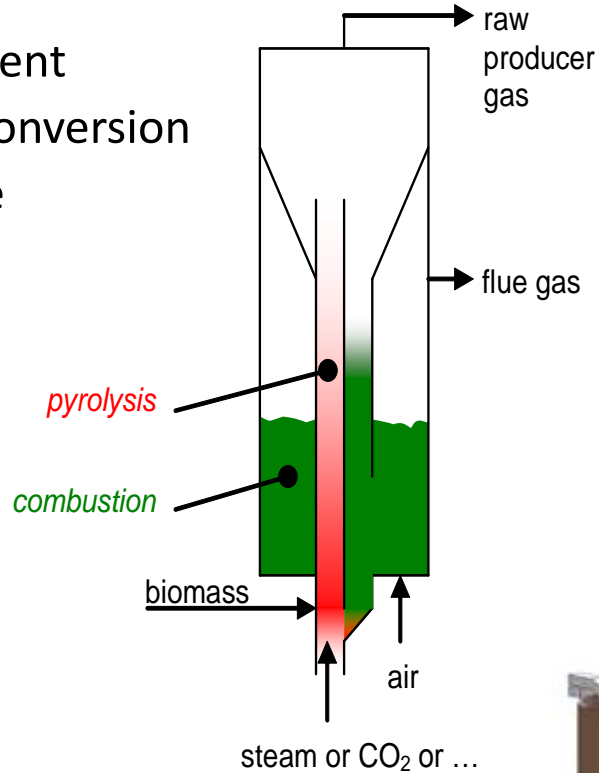
lower temperature, better efficiency, higher conversion



MILENA TECHNOLOGY

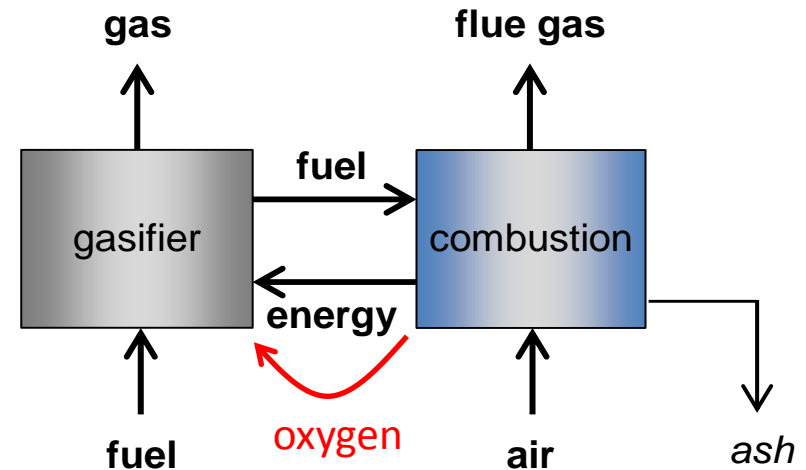
indirect gasification technology by ECN

- Highly efficient
- Complete conversion
- Fuel flexible
- Compact



INDIRECT GASIFICATION

- Energy transport between the two reactors
- Bed material takes carbon from gasifier to combustor
 - Char flows with bed material
 - Tars adsorb on (porous) bed material
 - CO₂ transport through carbonates
- Bed material can take oxygen from combustor to gasifier



OXYGEN TRANSPORT

description of the tests

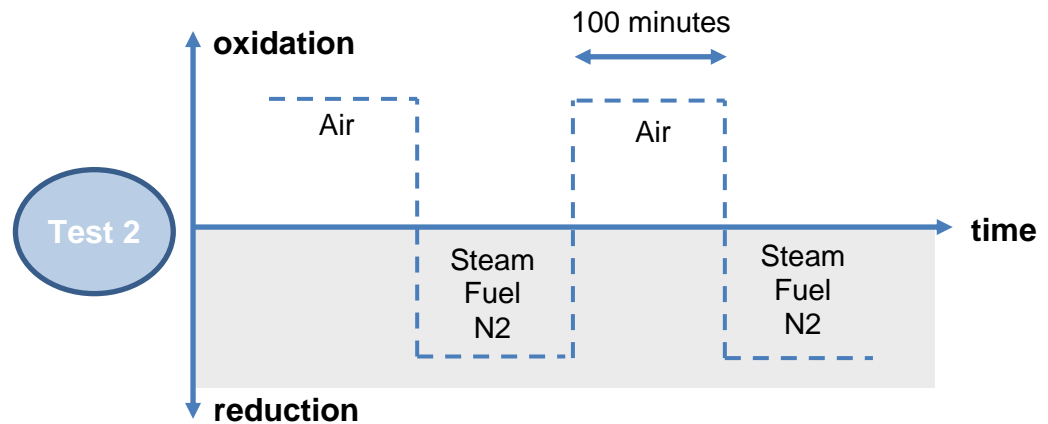
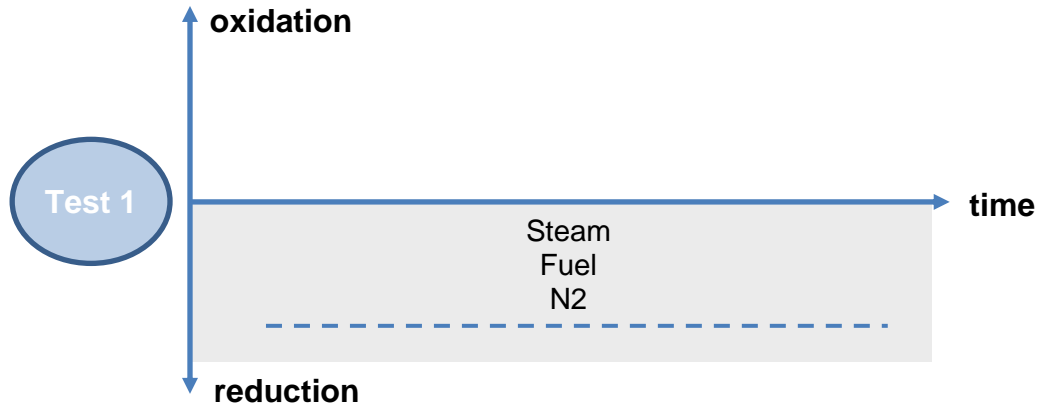
- Bubbling Fluidized Bed
- Olivine bed material (containing Fe)
- Clean wood fuel, 0.25 kg/h
- 880°C, 1 kg bed

- Two tests:
 - Test 1: only gasification
 - Test 2: intermittent gasification/combustion, 100 minutes cycle



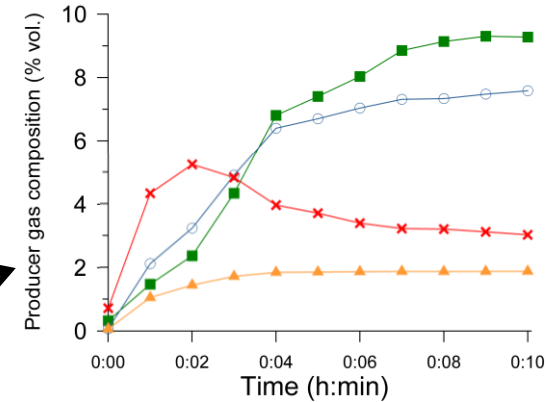
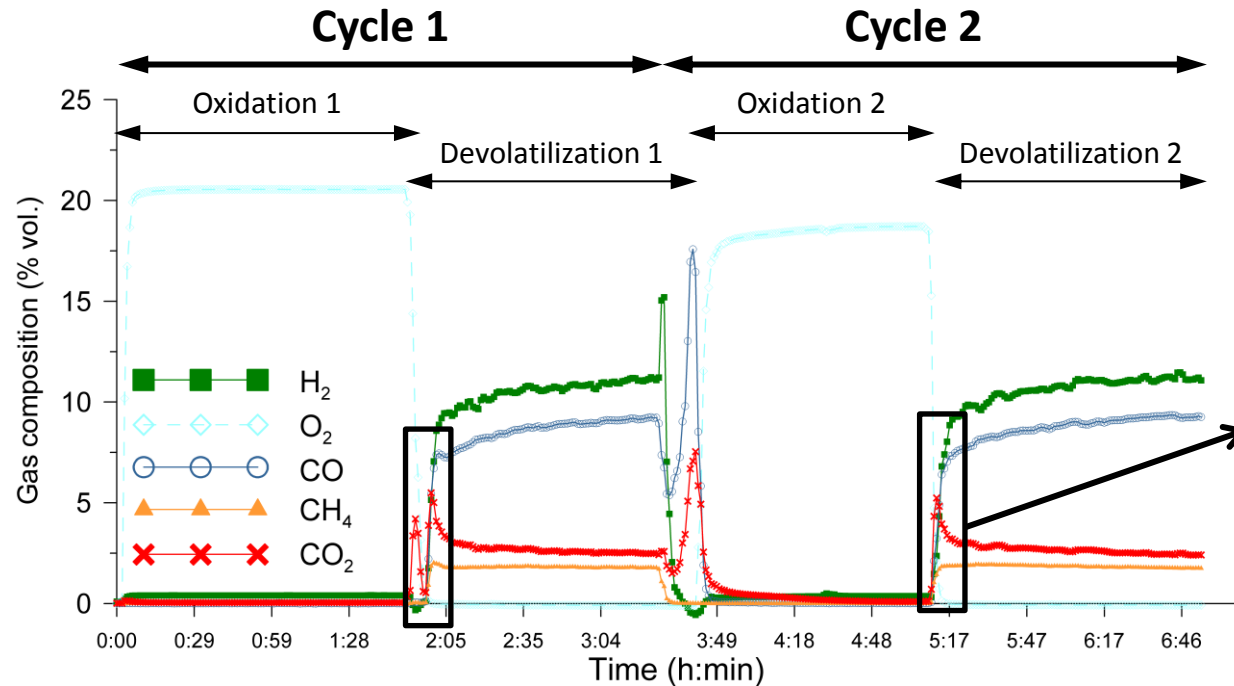
OXYGEN TRANSPORT

description of the tests



OXYGEN TRANSPORT

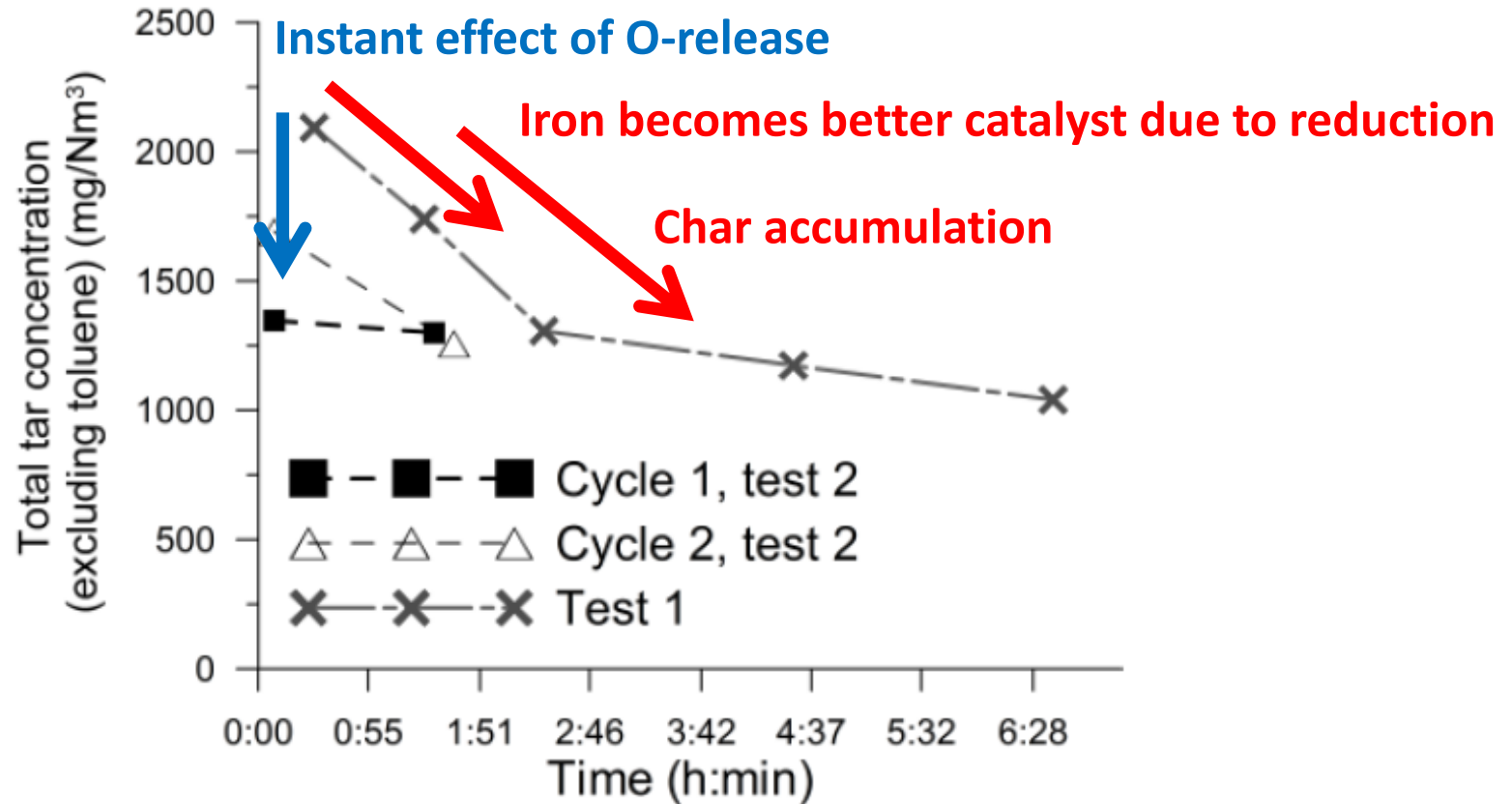
gas composition



Test 2

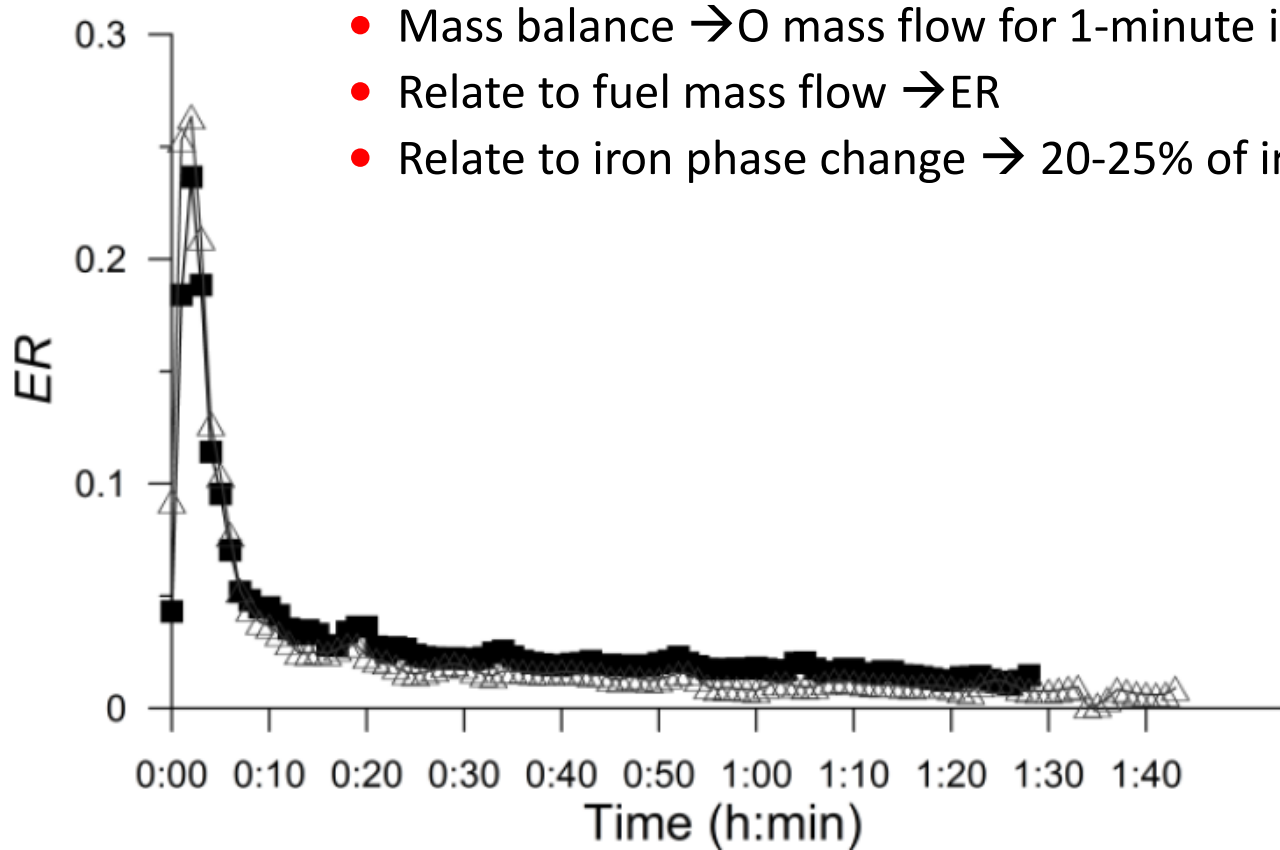
OXYGEN TRANSPORT

tars (by SPA method)



OXYGEN TRANSPORT

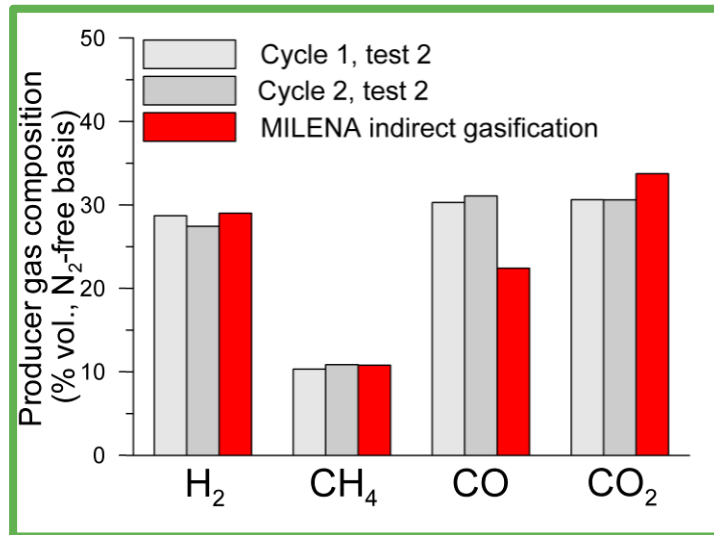
oxygen quantity



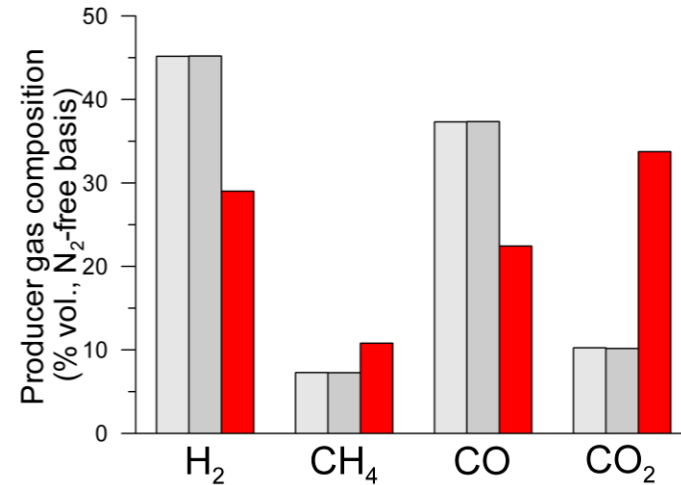
- Mass balance \rightarrow O mass flow for 1-minute intervals
- Relate to fuel mass flow \rightarrow ER
- Relate to iron phase change \rightarrow 20-25% of iron acts as O-pump

COMPARED TO MILENA

Test 2, first few minutes



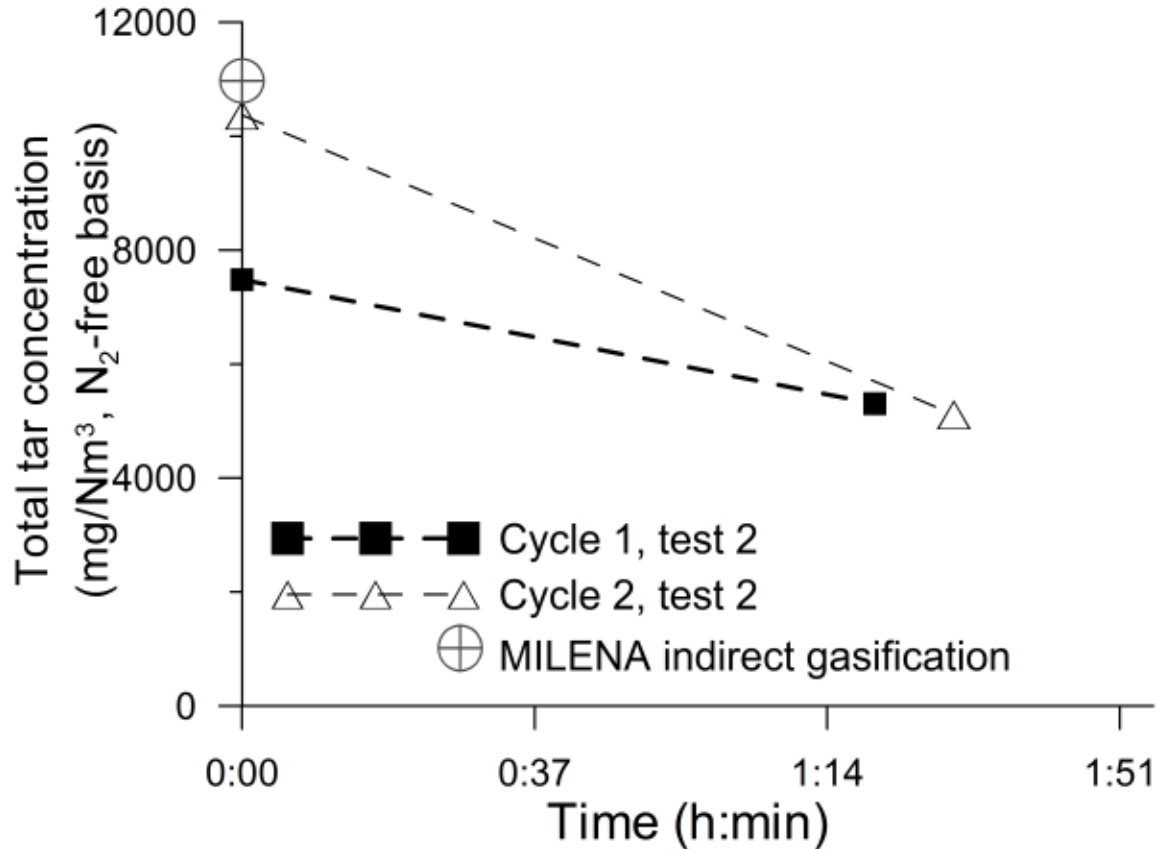
Test 2, after a while



MILENA operating conditions are equivalent to the initial point of maximum CO₂: olivine is kept at high oxygen transport capacity

OXYGEN TRANSPORT

compared to MILENA



CONCLUSIONS

- Indirect gasification offers degree of freedom compared to direct gasification, since unconverted carbon is not a loss: temperature
- Freedom to operate at low temperature means fuel flexibility
- Bed material in indirect gasification can transport oxygen through chemical looping
- This may add up to an ER of 0.2-0.3 during first few minutes of reduction
- This theoretically can supply all the required energy for gasification
- This also reduces tar:
 - By direct combustion of adsorbed tars on surface where iron reduces (O donor)
 - By increased gas phase reforming because of increased CO_2 and H_2O concentration
- MILENA is operated with fast reduction/short residence time: maximum oxygen transport

THANKS FOR THE ATTENTION

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www.ecn.nl

publications: www.ecn.nl/publications

fuel composition database: www.phyllis.nl

tar dew point calculator: www.thersites.nl

IEA bioenergy/gasification: www.ieatask33.org

Milena indirect gasifier: www.milenatechnology.com

OLGA: www.olgatechnology.com / www.renewableenergy.nl

SNG: www.bioSNG.com / www.bioCNG.com

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