

Towards a truly hybrid membrane for organic solvent filtration

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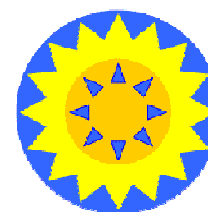
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M. Creatore (**Eindhoven University of Technology**)

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Towards a truly hybrid membrane for organic solvent filtration

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- ECN
- TUE
- Solsep BV

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SolSep BV



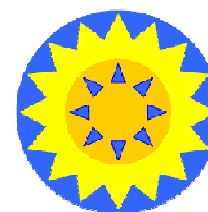
SolSep is an independent membrane producer (since 2000)

Focus on organic solvents

- mainly organic solvents
- some aqueous with x% solvent

SolSep

- produces membranes and SW elements
- not an equipment builder
- helps with development of applications (Organic solvent)



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Proven robustness in solvents

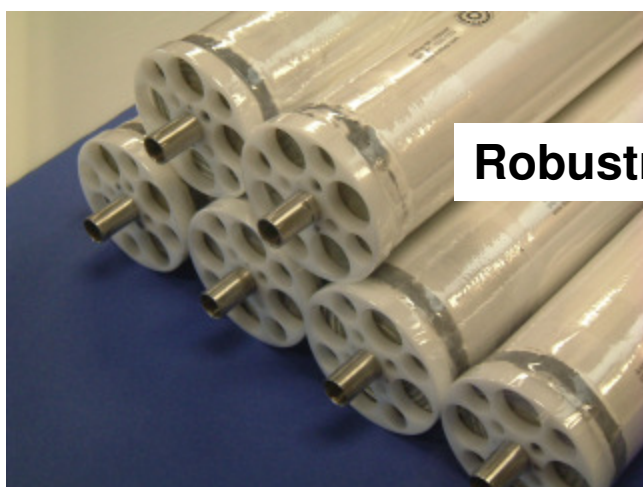
Technical grade solvents - may include water

All technical solvents:

hexane, ethyl acetate, acetone, MEK
ethanol, toluene, benzene, propylene oxide.....

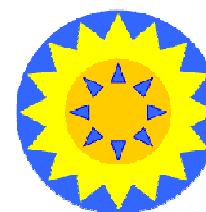
aprotic solvents NMP, THF, DMF, DMAc

water plus 10-20% solvent (EA, EthylE, polyether)



Robustness includes membranes and elements

SolSep Membranes

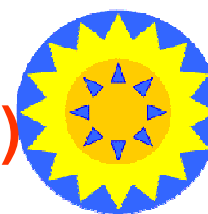


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		<i>Ultrafiltration</i>		<i>Nanofiltration</i>					
		010104	010706	010306	010206(S) ¹	030306	080105 ²	030705	030306F
Solvent systems	Alcohols	X	X	X	X	X	X	X	X
	Esters	X	X	X	X	X			
	Ketones	X		X		X	X	X	X
	Aromatics	X		X		X		X	X
	Chlorinated			X	X	X	X		X
	Red.Atmos.			X		X			

1. stabilized version for e.g aprotics
2. mainly for decolorization

Applications (decolorization-color harvesting)



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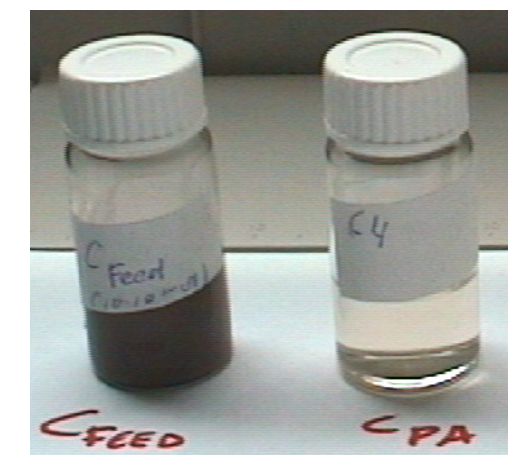
- Membranes are part of the solution
- Often combination of techniques



Fractionation of colors
In acetone and ethylalcohol

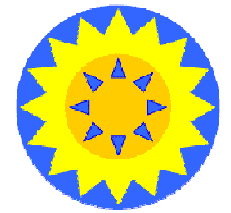


Natural colorant harvesting



Recovery of ethyl acetate

Processing examples



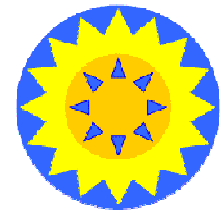
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Output 5-100 l/h



Output 200-2000L/h



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NF Membranes for organic solvents: what's there now



Polymeric membranes

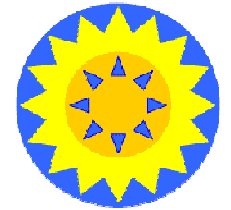
Ceramic membranes

Porous

Non-porous

- asymmetric

integrally skinned
composites



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What could be improved..?

Better agreement “expected” and real separation

partly not possible: see membranes in aqueous systems

partly improved by forecastable behavior

Causes of uncertainty (list is not complete...)

variable interaction in solvent-solute-membrane - swelling

pore-molecular “size” aspects

filtration/process aspects (CP, fouling)

Can we solve the problems?



Probably only partly

but we can check what is possible in some areas.

In this work: materials

combination of polymeric and ceramic

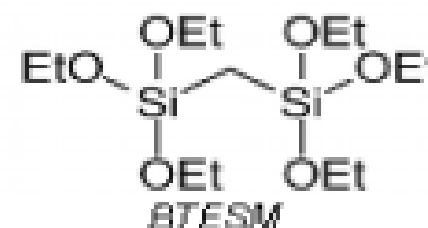
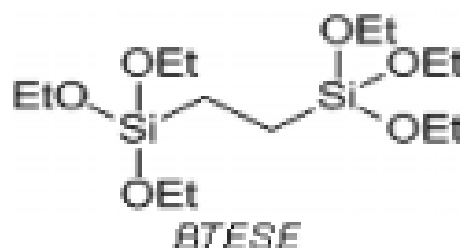
Lead: “Hybsi®” concept for pervaporation



HybSi® was developed for pervaporation (dehydration)

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HybSi ® = organic-inorganic hybrid silica-based amorphous material

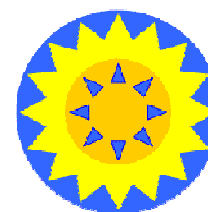


Very tight microporous materials
as such not useable as NF membrane

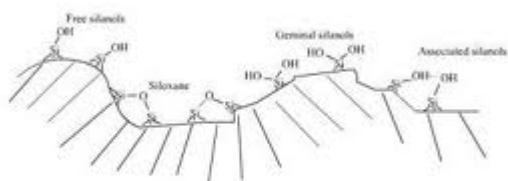
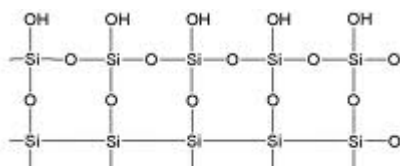
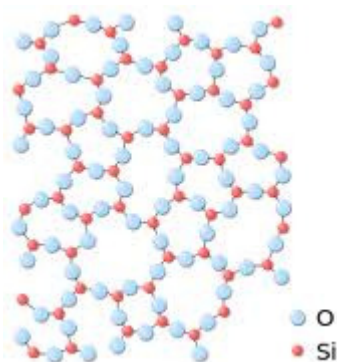
But –expected- to be very stable (in solvents)

“glassy polymer” where interaction plays an important role

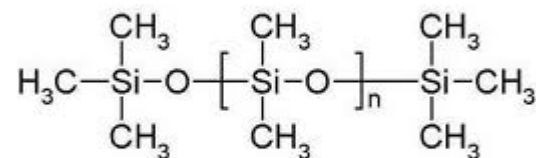
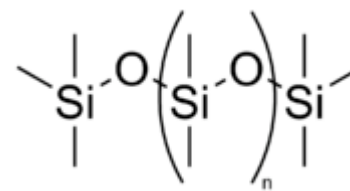
“Common” silicium containing polymers



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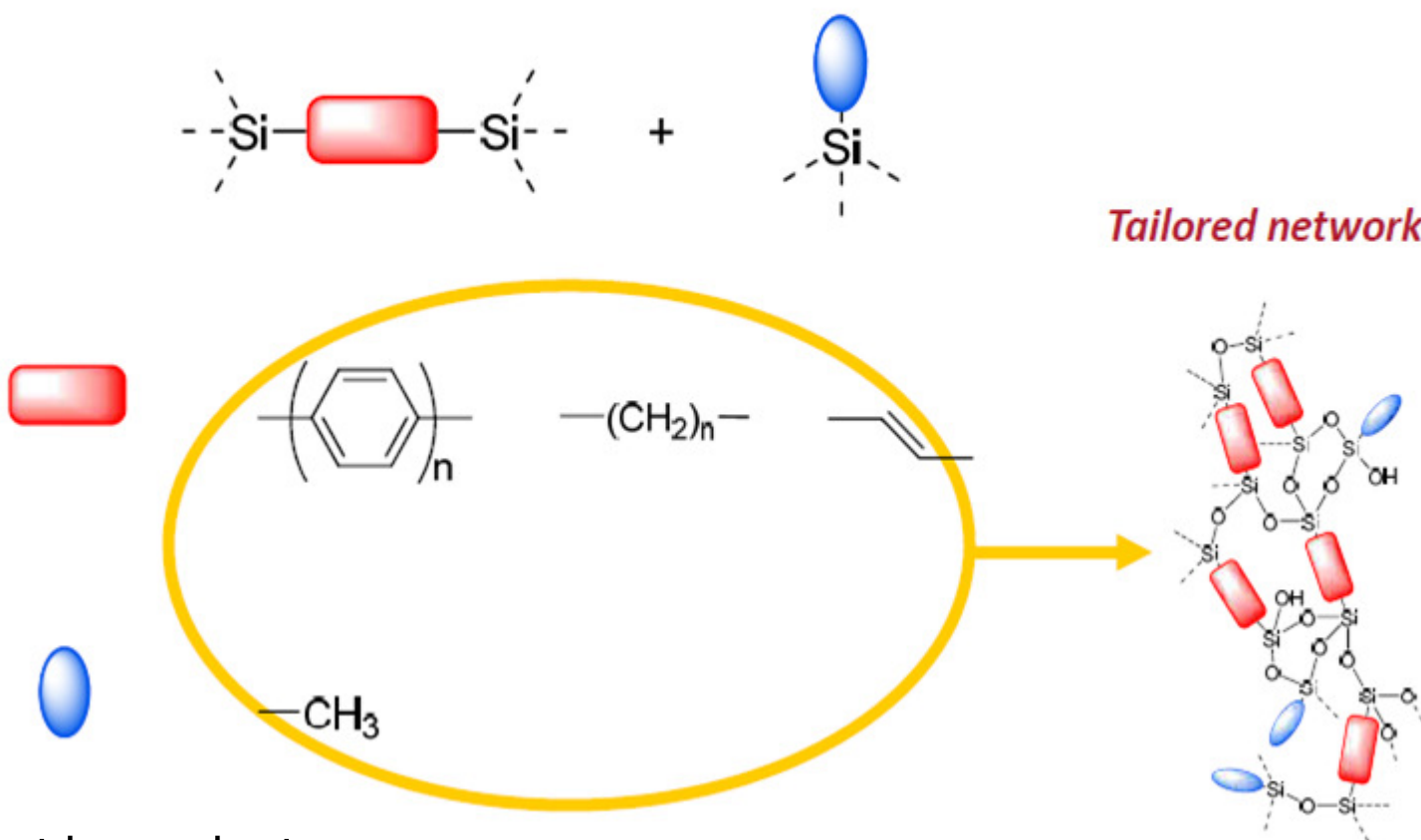


silica particle



siloxane

Precursors

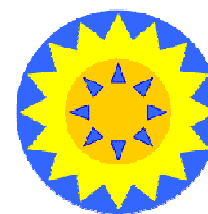


Concept in project:

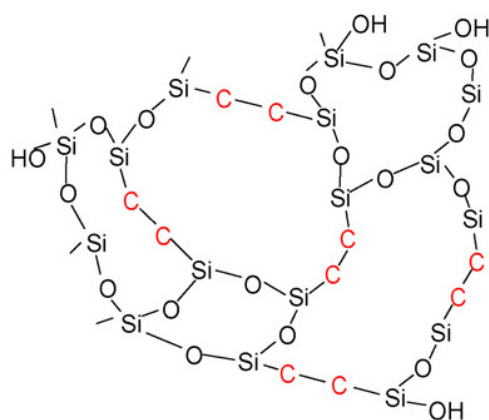
- HybSi types on polymeric substrates >>> scale up to SWEs
- vary blocks

www.SolSep.com use two deposition technologies

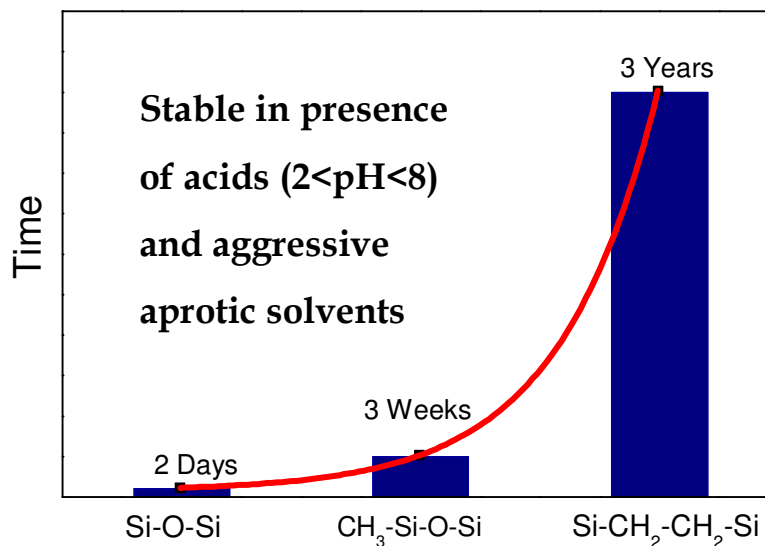
HybSi® in Pervaporation



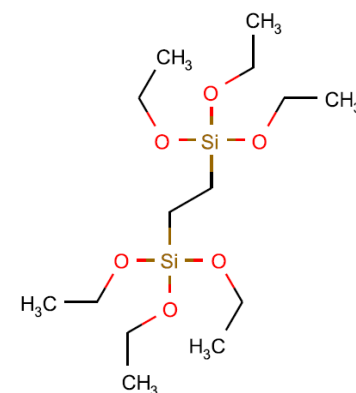
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Hybrid silica network



H.M. van Veen et al.; Journal of Membrane Science 380 (2011) 124-131.



1,2-Bis(triethoxysilyl)ethane (BTESE)

Si-**CH₂-CH₂**-Si bonds improve the **properties** of the silica network.

Can we make good membranes of “hybrid materials” on polymeric supports (better cost perspectives...) for NF??



Critical steps in synthesis

1) Sol-gel route “classical for membranes”

Sol synthesis (ECN)

Deposition on polymer sublayer >> semi ceramic system high T required

Post treatment

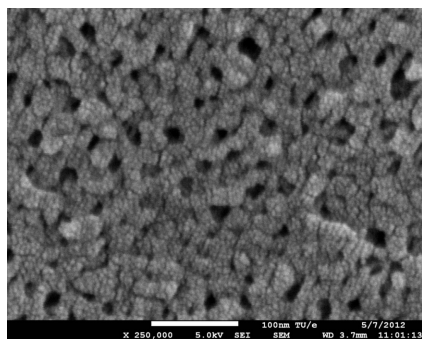
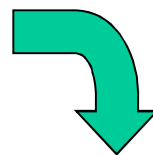
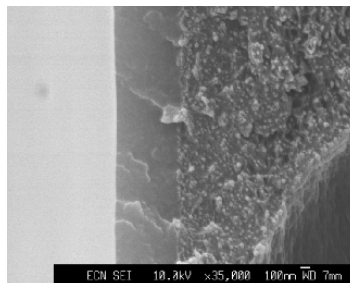
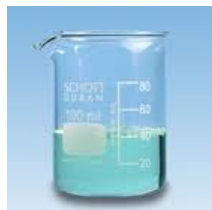
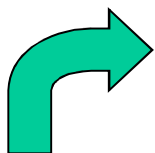
2) Plasma route “classical for polymer coats”

Reactive plasma (TUE)

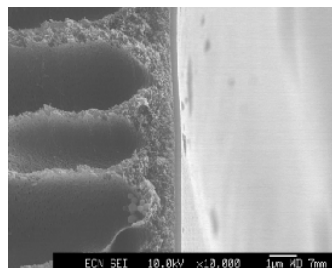
Deposition on stable layer (T, Chem stable)

Consistency in composition (initially close to HySi®)

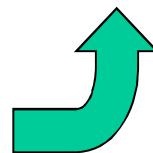
Flow scheme HybPON project

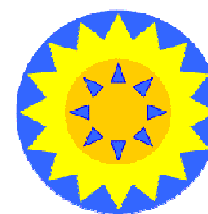


PI1109-0.3 (590 nm)



B (240 nm)





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Method #1: wet chemical deposition

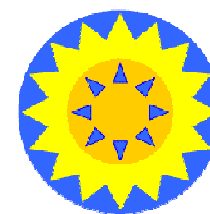


Membranes via sol-gel-Wet chemical deposition

- **HybSi (BTESE)**
 - Layers can be made
 - Sublayers were made that “survive” 150+degC
 - Very low P in NF
 - Have selectivity in PV
- **HybPON (BTESE + n-DTES) <-> stability of sol**
 - Layers can be made
 - Thin enough to give flexible stable membranes
 - Reasonable P, good-reasonable R in some solvent
- **Up-scaling**
 - Roll coating
 - Proof of principle

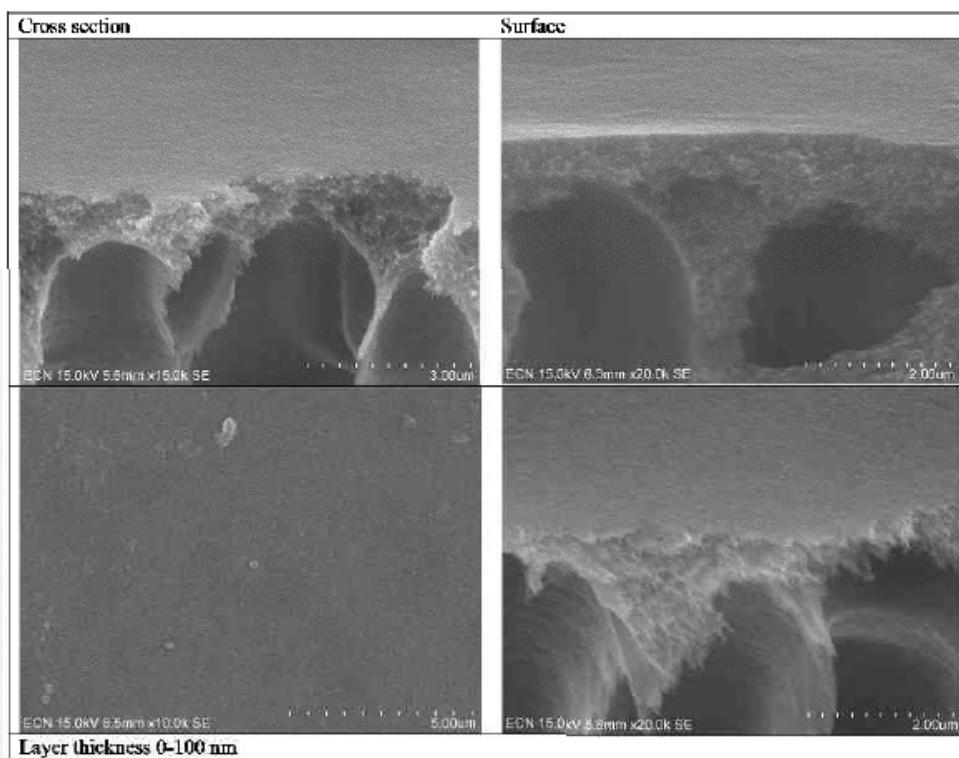
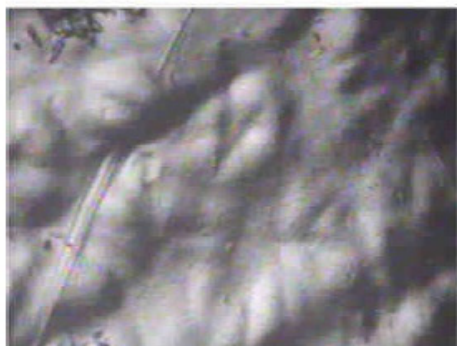


Coating – layer thickness



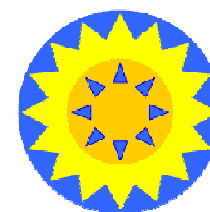
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1112-SOL BTESE+NDTES





Performance BETSE + n-DTES membrane on UF/NF supports

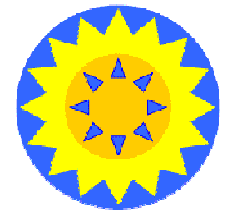


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			HybPON 0.3 M BTESE + n-DTES		SolSep 010206	
Solvent	Solute	Mw	Permeance	Retention	Permeance	Retention
Methanol			0.5			
	Methyl Red	269	0.3	adsorption	0.8	yes
	Bengaleroose	1018	0.1	yes		
Hexane			0		0	
	Sun Flower	900				
Toluene			0.3		0	
	Sun Flower	900	0.1	100%		
Acetone			1.3		2	
	Sun Flower	900	1.2	33%	1	100%

Permeance [l/m².hr.bar]

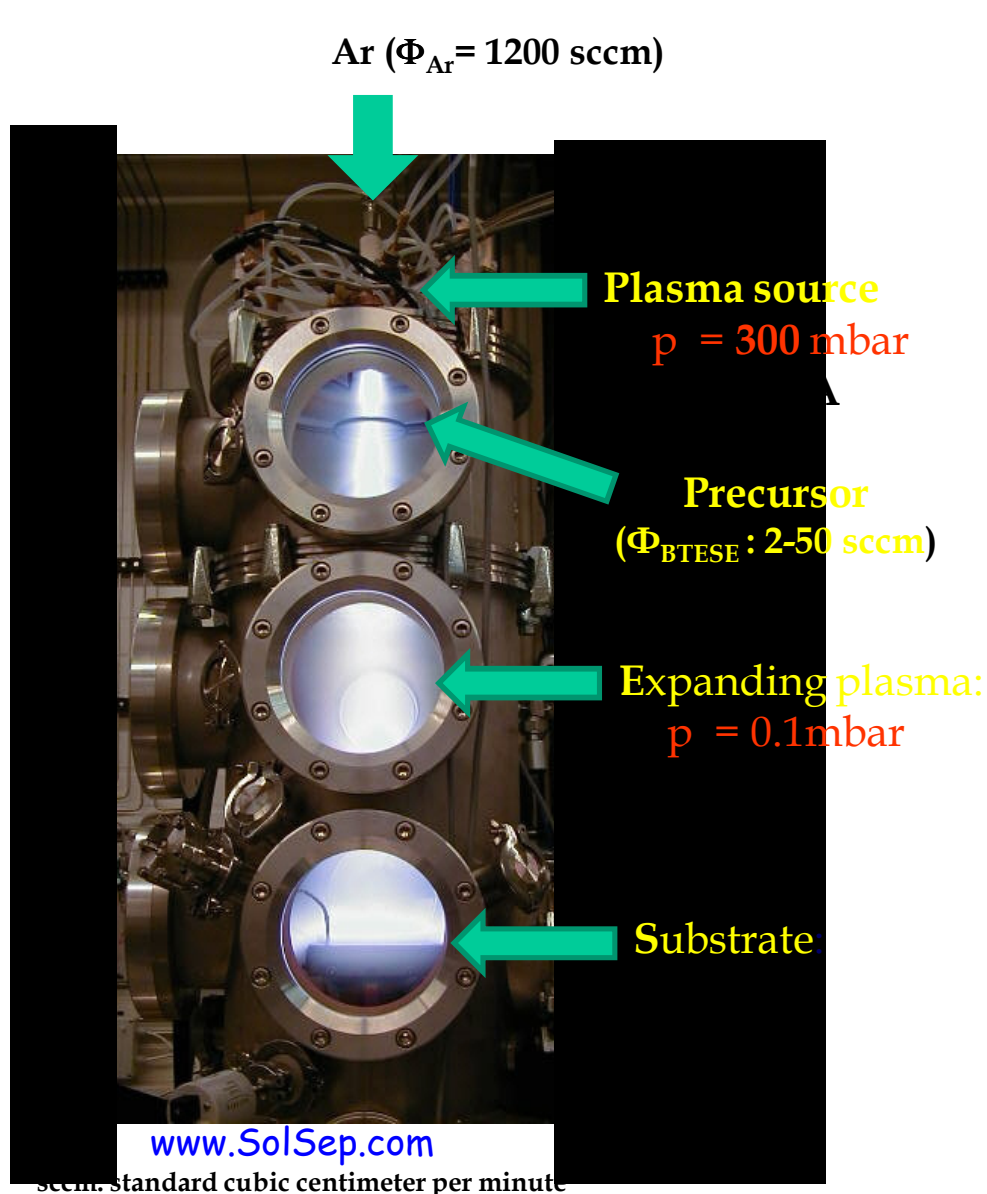
- HybPON membrane shows promising results in toluene
- Limited P



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Method #2 Plasma coating

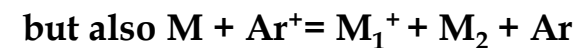
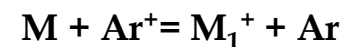
Experimental: The expanding thermal plasma - CVD



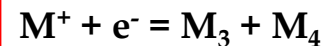
Industrial setup

Organosilicon/Ar Plasma chemistry

1- Charge exchange reaction



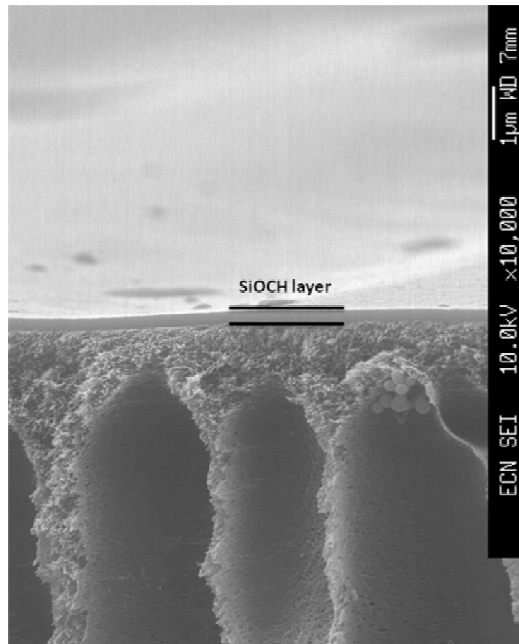
2- Dissociative recombination reaction



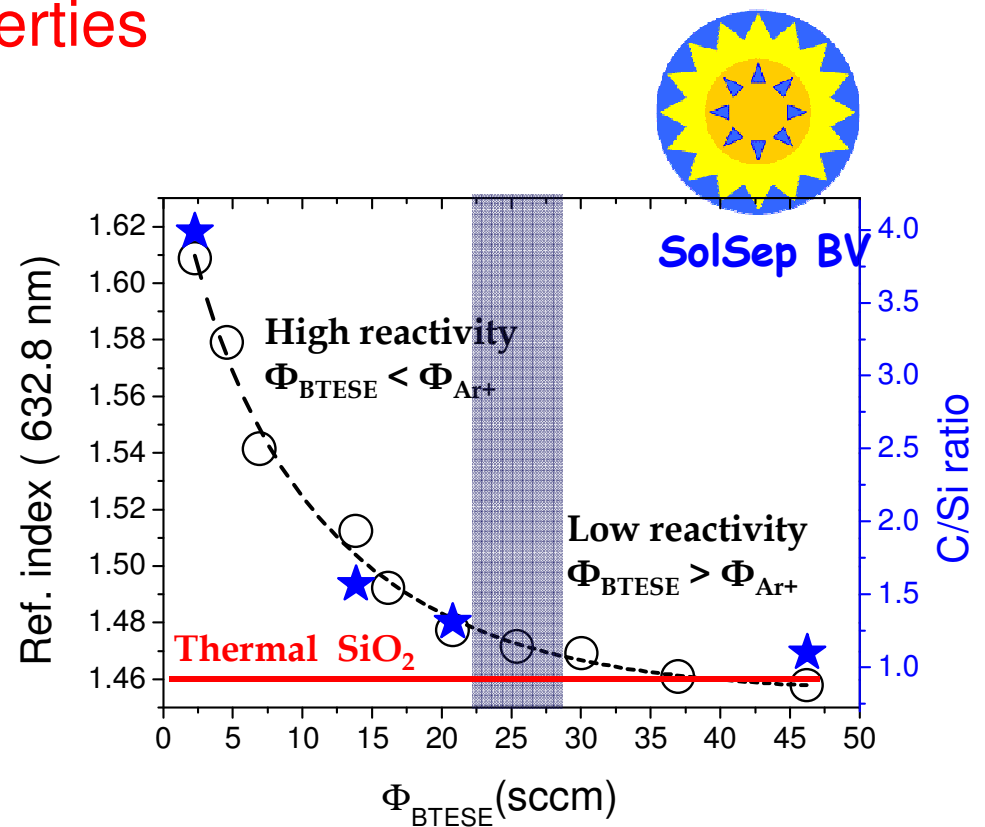
M_2 , M_3 and M_4 are radicals

M: Organosilicon precursor

Optical and chemical properties



Cross-sectional SEM image of the polyamide-imide-supported hybrid silica layer.



C/Si ratio is determined by Rutherford Back Scattering and the refractive index by Spectroscopic Ellipsometry.

As Φ_{BTESE} increases:

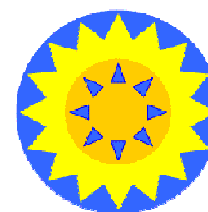
- Limited reactivity of the BTESE precursor
- Reduced film density and carbon content

Film density:

$\rho = 1.52 \text{ g/cm}^3$ @ 2.3 sccm

$\rho = 0.88 \text{ g/cm}^3$ @ 46.2.sccm

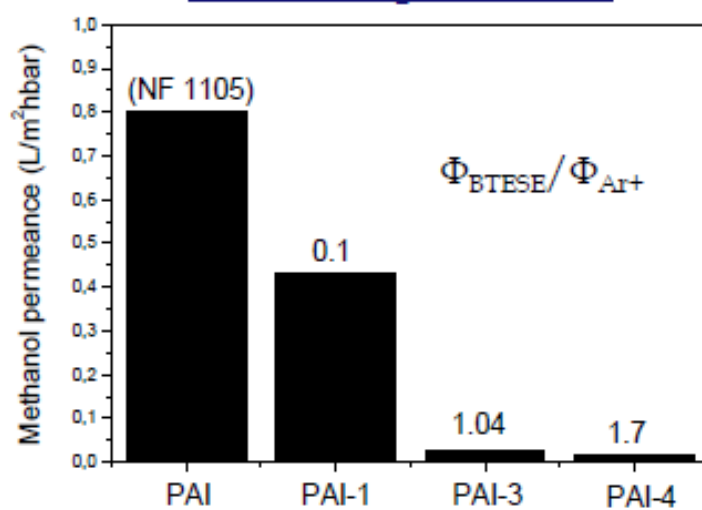
$\rho = 2.27 \text{ g/cm}^3$ (Thermal SiO_2)



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NF properties

Methanol permeance



Nanofiltration test

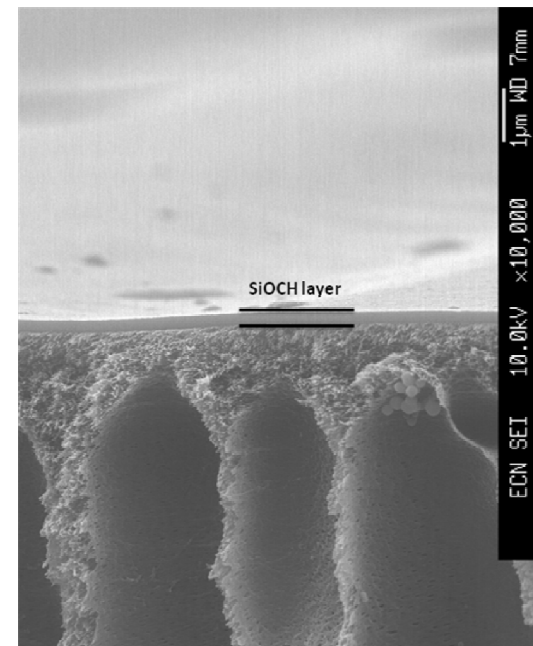


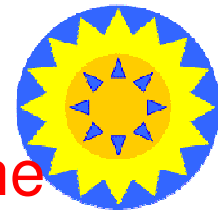
- Very low methanol permeance (too dense films)
- **Partial decolorization** of Methyl red (MW:269) in methanol.



Increase NF Permeance + R

- Optimize sublayer vs top layer thickness
- Small poresno pores (gutter layer)
- High porosity
- Low resistance
 - Large pores yield pin holes
 - Very thin layer gives more problems





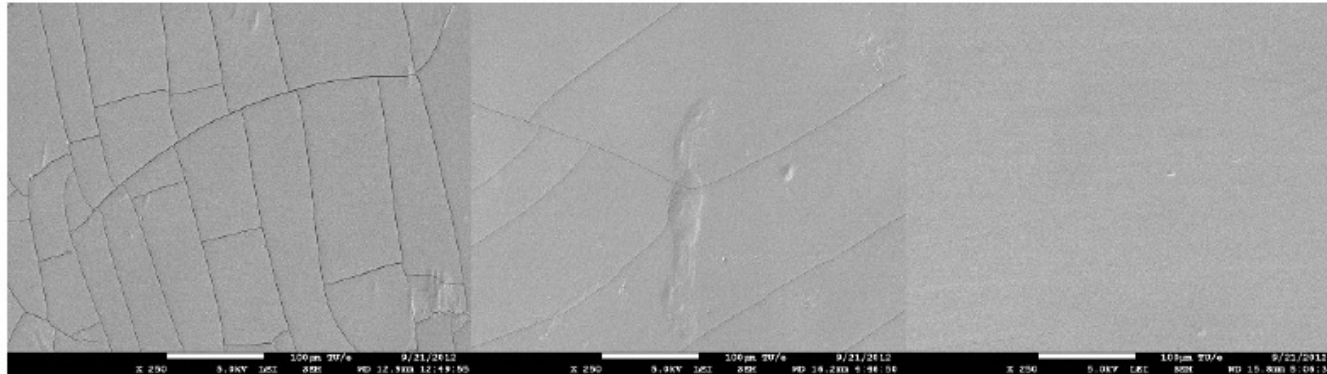
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Improving surface properties-effect on membrane

SiO₂ ($\approx 0.5 \mu\text{m}$)

SiO₂ ($\approx 0.5 \mu\text{m}$)/ PAI-3 ($\approx 250 \text{ nm}$)

SiO₂ ($\approx 0.5 \mu\text{m}$)/ PAI-3 ($\approx 600 \text{ nm}$)



SiO₂ ($\approx 0.5 \mu\text{m}$)/ PAI-3 ($\approx 1 \mu\text{m}$)

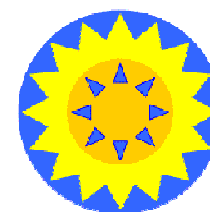
More cracks/defects at thicker layer

Use of intermediate layer >>

decreases cracks

Results

Plasma deposition on UF/PDMS



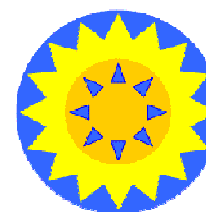
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Permeance [l/m².hr.bar]

Sublayer 1209S (UF/PDMS)

Solvent	Solute	Mw	PDMS	PAI-1	PAI-3	PAI-18
Methanol			0.2	0.06	0.05	
Hexane			8	0.02	0.05	
Toluene			12	0.1	0.05	0.47
	Sun Flower	900	7	0.04	0.02	0.14
			R=33%	R=0%	R=42%	R=100%

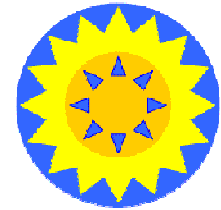
- Promising for toluene
- Plasma deposition on UF/BTESE+n-DTES deteriorated in methanol and acetone



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By the way- there is PV performance!

Membranes	WF (wt %)	$\alpha_{W/b}$	Water Flux (Kg/m ² h)	T(°C)	PSI*
PVA	5	<200	< 1.5	100	< 300
This work (Polymer- supported hybrid silica)	5	1133	2	95	2003
Hybsi ® (Ceramic- supported hybrid silica)	5	4700	3.6	95	16920



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Final remarks

- Semi-ceramic systems can be tailored towards NF membranes (HybPON vs HybSi®)
- Possible to make such systems onto polymeric supports – cost effective
- Can be done via -at least- 2 methods
- This opens up spiral wound manufacturing
- Good retention properties in some solvents
- Still not (yet?) “universal “

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